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Filter structure

The present invention relates to a pleated ion exchange adsorbent filter structure for removal of gaseous compounds in air and a process for production of such a filter structure.

Adsorption filters are used to remove undesired substances from gaseous or fluid mixtures. The present invention especially deals with filters for air filtration. Adsorbent particles, such as active carbon particles, fixed on a supporting frame clean undesired substances out of air carried through the filter. Modern industrial developments have resulted in increasingly stringent requirements with regard to clean air. Such industrial developments are, for example, the manufacture of highly sensitive products, such as semiconductors and microelectronic devices. This type of manufacture is performed in clean-rooms with extremely high demands for particle cleanliness. In the mid nineties the increasing miniaturization reached a level where also gaseous chemicals resulted in yield damage. These yield-damaging chemicals are denoted as airborne molecular contamination (AMC). Semiconductor Equipment and Materials International (SEMI) in the standard SEMI F21-951 have given a classification system for AMC gases. This standard divides AMC into four classes: Acids, Bases, Condensables and Dopants. Ion exchange adsorbents can be used to filter all types of acidic or alkaline substances.

The earlier conventional adsorption filters for removal of an acid compound, such as HCl or a basic compound, such as ammonia have relied on a chemical impregnation that is loosely bonded to its substrate. The impregnation may under some circumstances even result in a contamination itself. These chemically impregnated filters have in some cases much lower capacity than an ion exchange adsorbent filter.

Another type of adsorption filter incorporating ion exchangers has recently been developed, which uses ion exchanger particles. Such an ion exchanger containing adsorption

filter is described in US 6 402 819 B1. This filter comprises ion exchanger beads fixed to a support made of reticulated polymer foam or a textile web. In an adsorption filter using reticulated polymer foam as support, the adsorbent beads are fixed to the pore structure of the reticulated polymer foam. The pore structure of reticulated polymer foams has, due to its manufacture, a varying pore size, which leads to a varying adsorbent load. It is thus difficult to distribute the ion exchange beads evenly in the foam support, both in the surface direction and in the thickness direction. The adsorbent load also varies between different individual filters. Due to the uncertainty of the adsorbent load of the filters, only a minimum adsorbent load and thus a minimum filtration capacity can be guaranteed to the user. This is a significant problem, since a portion of the adsorbent, which is often very expensive, may be unused. The open structure of a foam support is indeed beneficial from a pressure drop standpoint, but it makes it impossible to achieve high initial removal efficiency at the short contact times between air and filter structure necessary to minimize pressure loss over the filter. Furthermore, since the adsorbent load of the foam support depends on the pore structure, it is not possible to fine-tune the adsorbent load versus efficiency versus pressure drop characteristics.

Another type of support for the ion exchanger beads that is also suggested in US 6 402 819 is a textile web. A textile web support has the advantage that it can be pleated, which is advantageous with respect to the pressure drop. However, problems occur when such textile web structures are to be pleated to a filter element and mounted in a filter panel frame, since the filter element will become distorted when used in the filtering application.

There is thus a need for an improved filter structure that does not suffer from the above drawbacks.

The object of the present invention is thus to provide an improved filter structure. This is achieved by a filter structure as described in claim 1, which can be pleated and which will not become distorted when used in the filtering application.

5 Summary of the invention

The present invention relates to a pleatable filter structure for use in a filter panel, containing ion exchange particles distributed within a fibrous framework. The filter structure is expanded so as to contain enough space to allow the ion exchange particles
10 to swell or to be in a swelled state as compared to dry ion exchange particles, without additional expansion of the filter structure.

In a preferred embodiment of the invention the fibrous framework of the filter structure comprises composite structural fibers (12) and composite thermoplastic fibers (18), the
15 composite structural fibers (12) comprising a first relatively higher melting component and a first relatively lower melting component, the first relatively higher melting component having a melting point at least 20 °C higher than the first relatively lower melting component, and the composite thermoplastic fibers (18) having a relatively
20 smaller denier than the structural fibers (12) and comprising a second relatively higher melting component and a second relatively lower melting component, wherein the composite structural fibers (12) form a thermally bonded, fibrous network in which the first relatively lower melting component bonds the structural fibers together at the
cross over points (14) to stabilize the fibrous network, and the composite thermoplastic
25 fibers (18) are dispersed throughout and bonded to the fibrous *network* by the application of heat so as to be immobilized, and wherein the ion exchange particles are bonded by the application of heat to the smaller denier composite thermoplastic fibers (18) and the filter structure is expanded so as to contain enough space to allow the ion
exchange particles to swell or to be in a swelled state as compared to dry ion exchange
30 particles, without additional expansion of the filter structure.

In one embodiment the expanded filter structure preferably contains enough space to allow an increase of the ion exchange particle diameter of at least 38 %, as compared to dry particles.

- 5 In one embodiment the filter structure contains enough space to allow an increase of the ion exchange particle diameter of at least 47 % as compared to dry particles.

In one embodiment the expansion of the filter structure has been achieved by a process in which the filter structure was exposed to a humid environment or water.

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In one embodiment the ion exchangers are macroporous polymers.

In one embodiment the load of ion exchangers is 100-2000 g/m², preferably 300-1000 g/m² and most preferably 400-700 g/m².

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In one embodiment the ion exchange particles are monospherical and has a diameter of 425-525 μm .

In one embodiment the fibrous framework comprises thermally bonded fibers.

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In one embodiment the fibrous framework comprises thermally bonded, fibrous network of coarse structural thermoplastic fibers and having fine thermoplastic fibers of relatively smaller denier than the structural fibers being dispersed throughout and bonded to the fibrous framework by the application of heat so as to be immobilized, wherein the ion exchange particles are bonded by the application of heat to the smaller denier composite thermoplastic fibers.

The present invention also relates to a filter panel in which the filter structure is pleated and fixed into a filter panel frame.

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In one embodiment the pleated filter structure has 0-25 pleats/dm, preferably 5-20 pleats/dm and most preferably 8-15 pleats/dm.

5 In one embodiment the height of the pleats is 10-300 mm, preferably 15-150 mm and most preferably 15-100 mm.

In one embodiment the frame is made of stainless steel or aluminum.

10 In one embodiment the pleated filter structure is fixed to the frame by means of a polyurethane adhesive, having a total outgassing lower than $10\mu\text{g/g}$, confirmed by thermal desorption gas chromatography mass spectroscopy (TD-GC-MS) with TD performed at 50°C for 30 min and n-decane as external standard.

15 In one embodiment exterior sealing strips for avoiding air bypass are made from a polymer having a total outgassing lower than $10\mu\text{g/g}$, confirmed by thermal desorption gas chromatography mass spectroscopy (TD-GC-MS) with TD performed at 50°C for 30 min and n-decane as external standard.

20 The present invention also relates to a method of manufacturing the filter structure according to claims 1-10, wherein a pleatable filter structure including ion exchange particles distributed in a fibrous framework, in which the pleatable filter structure is subjected to a moisture treatment in which it is exposed to a humid or water containing environment, whereby the ion exchanger particles swell and cause a permanent expansion of the filter structure.

25 In one embodiment the fibers of the fibrous framework are stretched as a result of the swelling of the ion exchange particles, and remain stretched.

30 In one embodiment the filter structure is exposed to this environment until the ion exchange particles have reached a moisture content of at least 20% by weight.

In one embodiment the filter structure is exposed to this environment until the ion exchange particles have reached a moisture content of at least 30 % by weight.

- 5 In one embodiment the ion exchange particles have a moisture content of less than 10 % prior to the moisture treatment and present an increase in diameter during the moisture treatment of up to 38 %.

- 10 In one embodiment the humid environment used in the moisture treatment has an absolute moisture content equivalent of a relative humidity of at least 70 % at a temperature.

- 15 In one embodiment the humid environment used in the moisture treatment has an absolute moisture content equivalent of a relative humidity of at least 80 %, preferably at least 90 % at a temperature of 30°C.

In one embodiment the filter structure is subjected to the moisture treatment in a batch process.

- 20 In one embodiment the filter structure is subjected to the moisture treatment in a continuous process.

Brief Description of the Drawings

- 25 Figure 1 is a representation of a cross-section through a filter structure of the present invention.

Figure 2 is a representation of a cross-section through a representative thermoplastic fiber of the present invention.

Figure 3 is a representation of a portion of the filter structure of Figure 1 showing

bonding of the fibers in the filter structure and bonding the ion exchange particles to the fibers of the filter structure.

Figure 4 shows the structure of a strong cation ion exchanger having $-\text{SO}_3\text{H}$ groups

Figure 5 shows the structure of a weak cation ion exchanger having $-\text{CH}_2\text{COOH}$ groups

Figure 6 shows the structure of a strong anion ion exchanger having $-\text{CH}_2\text{N}(\text{CH}_3)_3\text{OH}$ groups

Figure 7 shows a the structure of weak anion ion exchanger having $-\text{CH}_2\text{N}:(\text{CH}_3)_2$ groups

Figure 8 shows one example of a distorted pleat section of a filter panel

Figure 9 shows another example of a distorted pleat section of a filter panel

Figure 10 shows a finished panel after correct humidification and manufacture.

Figure 11 shows an equipment line for the manufacturing of a filter panel.

Detailed Description of the Preferred Embodiments

The ion exchange particulate filters of the present invention comprise a fibrous supporting framework in which the ion exchange particulate is distributed. The fibrous supporting framework may be of any type, as long as it contains fibers that are stretchable and have a low elasticity. This means that the fibers can be drawn out by means of a pulling force, and they do not return to their original state as the pulling force is released. Such fibers may be natural fibers or synthetic fibers.

The ion exchanger particles may be strongly acidic cation exchangers, weakly acidic cation exchangers, strongly basic anion exchangers or weakly basic anion exchangers (Figs 4-7). In strong cation exchangers the chemical groups are usually sulfonic acid groups, while strong anion exchangers may contain quaternary ammonium groups. The ion exchangers are preferably spherical beads of basic anion exchangers or acidic cation exchangers. They are usually in the form of spheres of a size of up to 1 millimeter. The spheres consist of macroporous or geltype polymers, mostly on the basis of sty-

rene, usually crosslinked in the form of styrene/divinylbenzene polymers bearing chemical groups with exchangeable ion functional groups, which permit the desired exchange. Macroporous polymers are preferred since they have desired porosity and have a greater ability to withstand structural damage at a variation in moisture content.

- 5 Ion exchange particles normally contain water. The water content of the ion exchange particles is influenced by the relative air humidity of the environment in which the particles are present. The higher the relative air humidity is, the more water is absorbed by the ion exchange particles. As the ion exchange particles absorb water, they increase in size, and they shrink when drying. At a relative humidity of 100 % the ion exchange
- 10 particles contain about 50 % by weight of water, and at a relative humidity of 50 % the ion exchange particles contain about 20 % by weight of water. There is thus an equilibrium between the relative air humidity and the water content, and consequently the size, of the ion exchange particles. However, it may sometimes take some time to reach the equilibrium water content of the ion exchange particles, depending on how they are
- 15 exposed to the humidity of the air.

- The water content of ion exchange particles in a filter cloth depends partly of the initial water content of the ion exchange particles, i.e. before incorporating the particles into the filter cloth. The manufacturing process of the filter cloth may also have a consider-
- 20 able influence on the ion exchange particle water content of the final filter cloth. Consequently, some filter cloths have ion exchange particles with a very low water content, and some have ion exchange particles with a higher water content. The water content of the ion exchange particles directly after the manufacture of the filter cloth is practically always lower (which means that the particle size is smaller) than the equilibrium water content of the ion exchange particles during the filtering application. In some
- 25 processes for manufacturing filter cloths, the ion exchange particles will be practically dry. In all processes were the degree of humidity of the ion exchange particulate is lower than in the intended application the resulting filter cloth cannot successfully be converted into a fixed pleated structure without previously being treated so as to

achieve an expansion of the fibrous framework, by the method of the present invention.

As the ion exchange particles constitute a chemically active media, the filter cloth is in all cases packed in more or less airtight packages before storage. The ion exchange particles thus remain in the state they were, i.e. very dry, after the manufacturing process until the filter cloth is to be used in a filtering application.

When the filter cloth is to be used as a filter element in a filter panel it must be pleated, in order to achieve satisfactory absorptive capacity and a sufficiently low pressure drop at the air speeds in question, which are normally between 0.3 and 3 m/s. If the filter cloth were pleated and fixed into a panel frame directly subsequent to the filter cloth forming process or directly after unpacking, it would distort severely when exposed to air of normal air humidity, i.e. air having a relative humidity of around 50 %, and even worse at higher relative humidities that are often the case in certain filtering applications. This distortion is due to the considerable swelling that the ion exchanger beads of the filter structure present when exposed to humidity. Since the ion exchanger beads are rather tightly entrapped in the fibrous framework, they have no free space to swell, and thus the swelling leads to an increase in size of the filter structure. the pressure that the ion exchanger convey to its surroundings is considerable, in a sealed vessel it can reach several 100 bars. The increase of the filter structure may be about 20% in area and thickness in a relative air humidity of 50%. Consequently, the pleated filter structure becomes too large to fit into the frame into which it is fixed, for which reason it becomes distorted. Examples of such distorted filter panel are shown in Figures 9 and 10.

The swelling of the ion exchanger beads proceeds gradually until the water content of the ion exchange particles is in equilibrium with the ambient air. A rolled up filter structure may be stored at normal air humidity for a long time without reaching an equilibrium between the moisture content of the ion exchanger beads and the ambient air. At 50 % relative air humidity, the ion exchanger beads will have a moisture content

of approximately 25 % by weight. When the moisture content of the ion exchanger beads increases from the initial practically dry state to 25 % by weight, as much as 80-85 % of the total possible increase in diameter takes place. This corresponds to a swelling of 160 % by volume. A saturated ion exchange particle contains about 50 % by weight of water and its diameter has increased 47 % as compared with a dry particle.

In order to avoid distortion of the pleated filter element in the resulting filter panel the filter structure is subjected to a moisturizing treatment, in which it is exposed to a humid or water containing environment prior to pleating. This moisturizing treatment or humidification step is performed by exposing the rolled out filter structure to clean air, i.e. air free of the substances that the filter structure intend to filtrate in the finished filter of certain humidity or by spraying it with a water aerosol. The humidifying treatment may be performed batch-wise in a chamber or as a continuous process step integrated in the apparatus in which the pleating of the filter structure is carried out. The relative humidity of the humidifying air should exceed the relative air humidity of the intended filtering application, preferably by 20 % in batch-wise treatment or by >20 in continuous treatment. For example, if the resulting filter panel is to be used in an application where the relative air humidity is 50 %, the humidifying air should have a relative air humidity of 70-80 %. The humidification is continued until the ion exchange particles of the filter cloth is in equilibrium with the humidity in the treating chamber or has reached a predetermined level in continuous treating operation. The relative humidity of air in a clean room, which is a particularly suitable application of the filter structure of the present invention, is usually 45-55%.

During the humidification the ion exchanger beads adsorb moisture from the humid air and swell to a certain degree that depends on the relative humidity of the humidifying air. As the ion exchanger particles swell, they stretch the fibers of the fibrous framework. The size of the space in which an ion exchanger particle is entrapped thus follows the size of the ion exchanger particles. The humidification is continued until the fibrous framework has reached the desired size, which means swelling of the ion ex-

change particles to a size slightly larger than size the ion exchange particles will reach in the actual filtering application. The fibrous framework has then been expanded to such an extent that the spaces can accommodate a swelled ion exchanger particle. The fibers of the fibrous framework are made of a comparatively inelastic material. The

5 stretching of the fibers and thus the expansion of the fibrous framework is thus a practically irreversible process, since the fibers do not return to their original non-stretched state. The expanded filter structure may now be directly pleated in a pleating equipment, cut and fixed into a filter panel frame. The expanded filter structure may also be stored until needed for the manufacture of a filter panel. In such a case a humidity con-
10 serving wrapping is most advantageous, since that ensures that the expanded filter structure does not contract or shrink. The finished filter panel may be stored in an environment having a lower relative humidity than the environment of the intended filtering application, the ion exchange particles may shrink to a smaller size. However, the ion exchanger particles remain secured within the fibrous framework, by adhesive or
15 by fusion points, depending on what type of filter cloth is used. Each space in the filter cloth that accommodates an ion exchange particle will then, apart from the ion exchange particle, contain an empty space. When the filter structure is once again exposed to the environment of higher relative humidity in the filtering application, the ion exchange particles return to their swelled state. This swelling does not cause any
20 expansion of the fibrous framework, since the spaces that accommodate the ion exchange particles are large enough to accommodate swelled ion exchanger particles. Such an expanded filter structure that is pleated and fixed into a filter panel, will thus not be distorted when exposed to the environment of the intended filtering application. The filter panel according to the present invention will thus not distort when used in
25 the desired filtering application and will also stand a drier or slightly more humid environment. In practice however, the filter panel would not be exposed to any large variations in air humidity, since it anyway has to be wrapped in order to protect the ion exchange particles from chemical components in the ambient air.

The moisture treatment can be used for all ion exchange filter cloths that have a fibrous framework containing fibers, which are stretchable and have a low elasticity.

A filter cloth that is particularly advantageous for the present application is described in EP 666 095 B1. This filter cloth has a high degree of dimensional stability. It in-

5 cludes a stable framework of relatively larger denier composite fibers, thermoplastic fibers of relatively smaller denier dispersed throughout and bonded to the framework, and an ion exchange particulate bonded to at least the smaller denier thermoplastic fibers. The larger denier fibers maintain the stability and permeability of the filter structure, which filter structure substantially is formed of the smaller denier fibers and the
10 particulate matter. The larger denier fibers should have a denier of at least about 30 dpf (denier per fiber) and should comprise a relatively higher melting component and a relatively lower melting component. The lower melting component bonds the fibers of the framework at the cross over points. The smaller denier fibers should have a denier of less than about 30 dpf and are dispersed throughout and bonded to the framework to
15 immobilize the thermoplastic fibers and to provide a surface for attachment of the ion exchange particulate. The ion exchange particulate is bonded to at least the smaller denier thermoplastic fibers.

This filter cloth is advantageous over fibrous filter cloths that contain an adhesive,
20 since the ion exchange particles are incorporated in the filter structure without the use of an adhesive. The use of adhesive has certain drawbacks, as will be discussed below. Firstly, the surface area of the ion exchanger will be partially covered by adhesive, which may substantially decrease the adsorptive effect of the filter. Secondly, an additional unwanted characteristic of adhesive containing filters is the well-known problem
25 of outgassing, i.e. that gaseous compounds are released from the filter panel itself, during use. Adhesives commonly used in the manufacture of ion exchange filter cloths have the disadvantage that they outgas AMC, such as medium and high boiling organic species, fire retardants, plasticisers and organophosphates.

By using a composite fiber cloth as the one described in EP 666 095 B1 an ion exchange adsorbent filter structure for use in filters for adsorption of acidic or alkaline airborne molecular compounds (AMC) from an air stream, having superior removal efficiency, superior capacity, a low pressure drop and which does not require the use of an adhesive to fix the adsorbent is provided.

The small and large denier fibers may be formed of the same material and may be sheath/core heterofilament fibers having a nylon sheath and a polyester core. A filter structure formed from such larger and smaller denier heterofilaments can be made having a thickness of from about 1,0 mm to 250 mm. The ion exchange particulate may have an effective particle diameter from 0,1 μm to 5 mm depending on the selection of the framework composite fibers and the smaller denier thermoplastic fibers.

This filter cloth is prepared by a method which comprises preparing a framework of the relatively larger denier composite fibers having a denier of 30 dpf or greater, and thermally bonding these fibers at the cross-over points. Smaller denier thermoplastic fibers are dispersed into the framework and these fibers have a denier of less than about 30. The smaller denier fibers are immobilized onto the framework and a particulate matter is dispersed onto the framework and thermally bonded to at least the smaller denier fibers.

The smaller denier fibers can be dispersed into the framework by hydro-entanglement or air-entanglement or some other suitable method. Alternatively, a web of relatively small denier thermoplastic fibers can be formed and larger denier fibers can be integrated into the smaller denier web to provide dimensional stability.

Figure 1 illustrates a cross-section through a portion of the filter structure used in the present invention. The filter structure includes a stable framework of relatively larger denier composite structural fibers 12 that are thermally bonded at the cross over points 14. By the term "structural fibers" is meant fibers of relatively larger denier that may

be used to support a filter or fabric structure. These structural fibers have a denier of at least about 30 dpf.

5 The structural fibers may range in denier from about 30 dpf to 10,000 dpf or larger depending on the stiffness desired for providing a framework that is resistant to compression and is otherwise dimensionally stable and the size of the functional particulate 16 that is chosen. The composite fibers should be present in an amount sufficient to provide a structure to which may be bonded the relatively smaller denier fibers 18.

10 The composite fibers 12 have a higher melting component and a lower melting component. The higher melting component has a melting point at least about 20°C higher than the relatively lower melting component. When heated above the melting point of the lower melting component, but below the melting point of the higher melting component, the lower melting component bonds the fibers of the framework together with-
15 out affecting the structural integrity of the framework that is provided by the higher melting component.

Composite fibers suitable for use as structural fibers in the practice of the invention include bi-component fibers in which the higher and lower melting components are arranged in a side-by-side relationship, or heterofilament fibers having either a concentric or eccentric sheath/core arrangement with the high melting component forming the
20 core and the lower melting component forming the sheath. The term "heterofilaments" as used herein refers to both staple fiber and to continuous filament, unless otherwise specified. The term "fiber" as used herein also refers to both cut staple and to continuous filament, unless otherwise specified. In side-by-side fibers the two components, one higher melting and one lower melting, are simultaneously extruded through single orifice to form a fiber having two halves. In the concentric sheath/core arrangement, a higher melting component forms a core centered axially within a lower melting sheath. In the eccentric sheath/core arrangement, the higher melting component is not centered
25 axially of the fiber. Composite fibers are also sometimes referred to as bicomponent
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fibers.

Composite fibers having a lower melting nylon component and a higher melting polyester component have been found useful in the practice of the invention. For example, a sheath/core heterofilament (Figure 2) having a nylon sheath with a melting point from about 175-185 °C and a polyester core with a melting point of from about 240-256 °C has proven to be useful in the practice of the present invention.

Figure 2 is a representation of a cross-section through a heterofilament 20. Heterofilament fiber 20 is representative of the many types of composite manufactured fibers that may be used for the framework or for attachment of the active particulate of the filter structure shown at 10 in Figure 1.

Fiber 20 is illustrated as a concentric sheath-core heterofilament fiber in which the sheath and the core each comprise about 50% of the cross-sectional area of the fiber. A range of area of the fiber occupied by the sheath is contemplated to be from about 20 to about 80%. The fiber has a lower melting nylon sheath 22 and a higher melting polyester core 24. The sheath should have a melting point that is at least about 20 °C below the melting point of the core and should occupy about half the cross-section of the fiber to provide strong thermal bonding of the fiber structure without adversely affecting the integrity of the core. The core provides strength and integrity to the filter structure.

The framework of relatively large denier structural fibers 12 of the filter structure of the invention all include composite manufactured fibers as described above, having a lower melting component for thermal bonding of the structure at cross over points 14 and for immobilizing relatively smaller denier fibers 18. The skilled artisan should recognize that there are a wide variety of composite fibers having a higher melting component and a lower melting component that are suitable for the practice of the invention and that a heterofilament fiber having a nylon sheath and a polyester core is but

one of the broad array of fibers available. The composite fibers 12 may also be in a wide variety of forms including crimped and non-crimped cut staple fibers, short cut staple, continuous filaments or blends thereof.

- 5 Smaller denier thermoplastic fibers 18 of the filter structure 10 are immobilized on the framework of larger denier fibers and provide, in addition to the particulate matter, active filtration of liquids and gases. These smaller denier fibers also greatly increase the surface available for immobilizing the functional particulates. These smaller denier fibers can range in denier from about 1 to 30 dpf. Smaller denier staple fibers and short
- 10 cut staple are particularly useful in the filter structure of the invention, although continuous filaments are also contemplated. Fibers 18 should be present in an amount sufficient to immobilize the particulate matter and to provide a desired filtration at an acceptable pressure drop across the filter.
- 15 The smaller denier thermoplastic fibers can be immobilized in the framework of larger denier fibers through the application of heat. Care should be exercised to avoid fusing the smaller fibers into a mass that could adversely impact pressure drop across the filter or otherwise reduce filter efficiency. It has been found useful in the practice of the invention to use smaller denier fibers that have the same components as the composite
- 20 structural fibers forming the framework.

For example, if sheath/core heterofilaments of nylon and polyester are used to form the framework, then it is useful for bonding the structure and for immobilizing the smaller diameter fibers and the particulate matter if the smaller denier fibers are also

25 sheath/core heterofilaments of nylon and polyester having similar melting points. This similarity in melting points simplifies bonding of the filter framework, bonding of the smaller diameter fibers to the framework, and bonding of the particulate matter to the filter structure. Bonding and immobilization of the smaller denier fiber to the larger denier fiber, and fusing of the particulate matter to the larger and smaller denier fibers,

30 is much the same as described herein above with respect to the bonding the larger

denier composite fibers to form a framework.

Figure 3 is a greatly enlarged representation of an ion exchange particle 16 immobilized within a framework of larger denier and smaller denier fibers 12 and 18, respectively. The smaller denier fibers are immobilized on the framework of larger denier fibers at numerous points 26. The particles are fused primarily to the smaller denier fibers at numerous points 28, and may also be bonded to the larger denier fibers as shown at 30. As can be seen from Figure 3, the filter structure is a cage-like structure in which particulate matter may be entrapped and substantially precluded from migrating. Fusing of the particle to the individual fibers desirably is localized in that the fiber does not form a film over the particle or otherwise substantially reduce the surface area of the particle available for contact with a liquid or gas stream moving through the filter structure.

The composite fiber filter cloth may be produced by a variety of alternative processes, which are described in EP 066095 B1.

The method for expanding the filter cloth so as to form the filter structure of the present invention may be carried out batch-wise or continuously.

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In the case of batch-wise humidification the filter cloth is exposed to humid air in a humidification chamber. The humidity of the air in the humidification chamber is preferably 70 % and the time for exposure of the filter cloth to humid air is between 4 and 6 hours.

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In a continuous humidification process the filter cloth is transported through a humidifying tunnel, in which the humidifying air preferably has a relative humidity of 80-100 %. The temperature is 20-60°C and the exposure time is 1-10 minutes.

The moisture treatment can also be carried out by spraying a water aerosol on to the filter cloth.

5 The humidification step is followed by pleating of the filter structure, cutting it to the desired dimension and attaching it to the panel frame by means of an adhesive.

10 In order to achieve a filter panel with low outgassing, i.e. a low amount of gaseous compounds that are released from the filter panel itself, during use, the adhesive should be a polyurethane adhesive, having a total outgassing lower than 10 $\mu\text{g/g}$, confirmed by thermal desorption gas chromatography mass spectroscopy (TD-GC-MS), with TD performed at 50 °C for 30 min and n-dodecane as external standard.

15 Figures 8 and 9 show examples of distorted pleat sections of filter panels. The filter structures of these filter panel were not subjected to a moisture treatment according to the present invention and did thus not contain any free space for the ion exchange particles to swell. As these pleated filter structures were exposed to humid air in a filtering application, the pleats have thus become deformed.

Figure 10 shows a finished panel after correct humidification and manufacture.

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An equipment line for the manufacturing of a filter panel is shown in Figure 11. This equipment line comprises an unwinding stand (A), a humidifier (B), a pleater (C) and a pleat pack treatment table (D).

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Claims

1. Pleatable filter structure for use in a filter panel, containing ion exchange particles distributed within a fibrous framework,

5 **characterised in** that the filter structure is expanded so as to contain enough space to allow the ion exchange particles to swell or to be in a swelled state as compared to dry ion exchange particles, without additional expansion of the filter structure.

10 2. The filter structure of claim 1, wherein the fibrous framework comprises composite structural fibers (12) and composite thermoplastic fibers (18), the composite structural fibers (12) comprising a first relatively higher melting component and a first relatively lower melting component, the first relatively higher melting component having a melting point at least 20 °C higher than the first relatively lower melting component, and the composite thermoplastic fibers (18) having a relatively smaller denier than the
15 structural fibers (12) and comprising a second relatively higher melting component and a second relatively lower melting component, wherein the composite structural fibers (12) form a thermally bonded, fibrous network in which the first relatively lower melting component bonds the structural fibers together at the cross over points (14) to stabilize the fibrous network, and the composite
20 thermoplastic fibers (18) are dispersed throughout and bonded to the fibrous *network* by the application of heat so as to be immobilized, and wherein the ion exchange particles are bonded by the application of heat to the smaller denier composite thermoplastic fibers (18) and the filter structure is expanded so as to contain enough space to allow the ion exchange particles to swell or to be in a swelled state as compared to dry ion exchange particles, without additional expansion of the filter structure.

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30 3. The filter structure of claim 1 or 2, wherein the expanded filter structure contains enough space to allow an increase of the ion exchange particle diameter of at least 38 % as compared to dry particles.

4. The filter structure of any one of claims 1-3, wherein the expanded filter structure contains enough space to allow an increase of the ion exchange particle diameter of at least 47 % as compared to dry particles:

5 5. The filter structure of any one of claims 1-4, wherein the expansion of the filter structure has been achieved by a process in which the filter structure was exposed to a humid environment or water.

6. The filter structure of any one of claims 1-5, wherein the ion exchangers are macro-
10 porous polymers.

7. The filter structure of any one of claims 1-6, wherein the load of ion exchangers is 100-2000 g/m², preferably 300-1000 g/m² and most preferably 400-700 g/m².

15 8. The filter structure of any one of claims 1- 7, wherein the ion exchange particles are monospherical and has a diameter of 425-525 μ m.

9. The filter structure of any one of claims 1- 8, wherein the fibrous framework comprises thermally bonded fibers.

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10. The filter structure of any one of claims 1-9, wherein the fibrous framework comprises thermally bonded, fibrous network of coarse structural thermoplastic fibers and having fine thermoplastic fibers of relatively smaller denier than the structural fibers being dispersed throughout and bonded to the fibrous framework by the application of heat so as to be immobilized, wherein the ion exchange particles are bonded by the application of heat to the smaller denier composite thermoplastic fibers.

11. A filter panel comprising the filter structure of any one of claims 1-10, wherein the filter structure is pleated and fixed into a filter panel frame.

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12. The filter panel of claim 11, wherein the pleated filter structure has 0-25 pleats/dm, preferably 5-20 pleats/dm and most preferably 8-15 pleats/dm.

13. The filter panel of claim 11 or 12, wherein the height of the pleats is 10-300 mm, preferably 15-150 mm and most preferably 15-100 mm.

14. The filter panel of any one of claims 11-13, wherein the frame is made of stainless steel or aluminium.

15. The filter panel of any one of claims 11-14, wherein the pleated filter structure is fixed to the frame by means of a polyurethane adhesive, having a total outgassing lower than 10 $\mu\text{g/g}$, confirmed by thermal desorption gas chromatography mass spectroscopy (TD-GC-MS), with TD performed at 50 °C for 30 min and n-decane as external standard.

16. The filter panel of any one of claims 11-15, wherein exterior sealing strips for avoiding air bypass are made from a polymer having a total outgassing lower than 10 $\mu\text{g/g}$, confirmed by thermal desorption gas chromatography mass spectroscopy (TD-GC-MS) with TD performed at 50 °C for 30 min and n-decane as external standard.

17. Method of manufacturing the filter structure according to claims 1-10, wherein a pleatable filter structure including ion exchange particles distributed in a fibrous framework, characterized in that the pleatable filter structure is subjected to a moisture treatment in which it is exposed to a humid or water containing environment, whereby the ion exchanger particles swell and cause a permanent expansion of the filter structure.

18. The method of claim 17, wherein the fibers of the fibrous framework are stretched as a result of the swelling of the ion exchange particles, and remain stretched.

19. The method of any one of claims 17-18, wherein the filter structure is exposed to this environment until the ion exchange particles have reached a moisture content of at least 20% by weight.

5 20. The method of any one of claims 17-19, wherein the filter structure is exposed to this environment until the ion exchange particles have reached a moisture content of at least 30 % by weight.

10 21. The method of any one of claims 17-20, wherein the ion exchange particles have a moisture content of less than 10 % prior to the moisture treatment and present an increase in diameter during the moisture treatment of up to 38 %.

15 22. The method of any one of claims 17-21, wherein the humid environment used in the moisture treatment has a relative humidity of at least 70 % at a temperature of 20 °C.

20 23. The method of any one of claims 17-22, wherein the humid environment used in the moisture treatment has a relative humidity of at least 80 %, preferably at least 90 % at a temperature of 30 °C.

24. The method of any one of claims 17-23, wherein the filter structure is subjected to the moisture treatment in a batch process.

25 25. The method of any one of claims 17-23, wherein the filter structure is subjected to the moisture treatment in a continuous process.



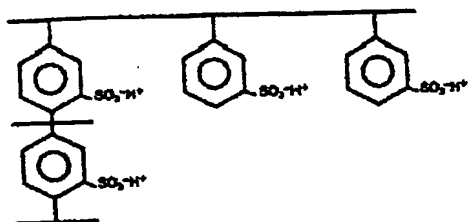


FIG 4

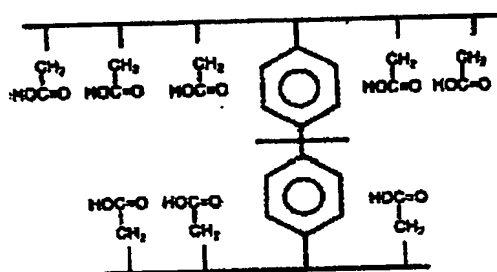


FIG 5

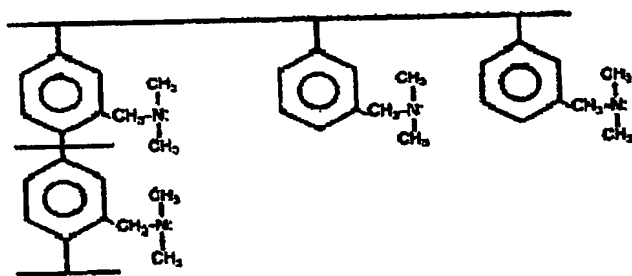


FIG 6

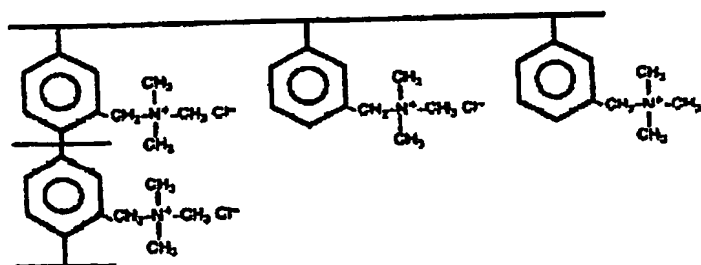


FIG 7

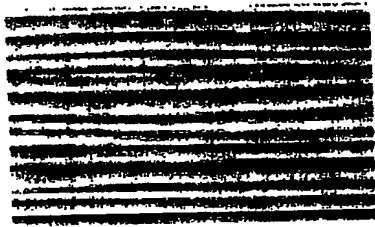
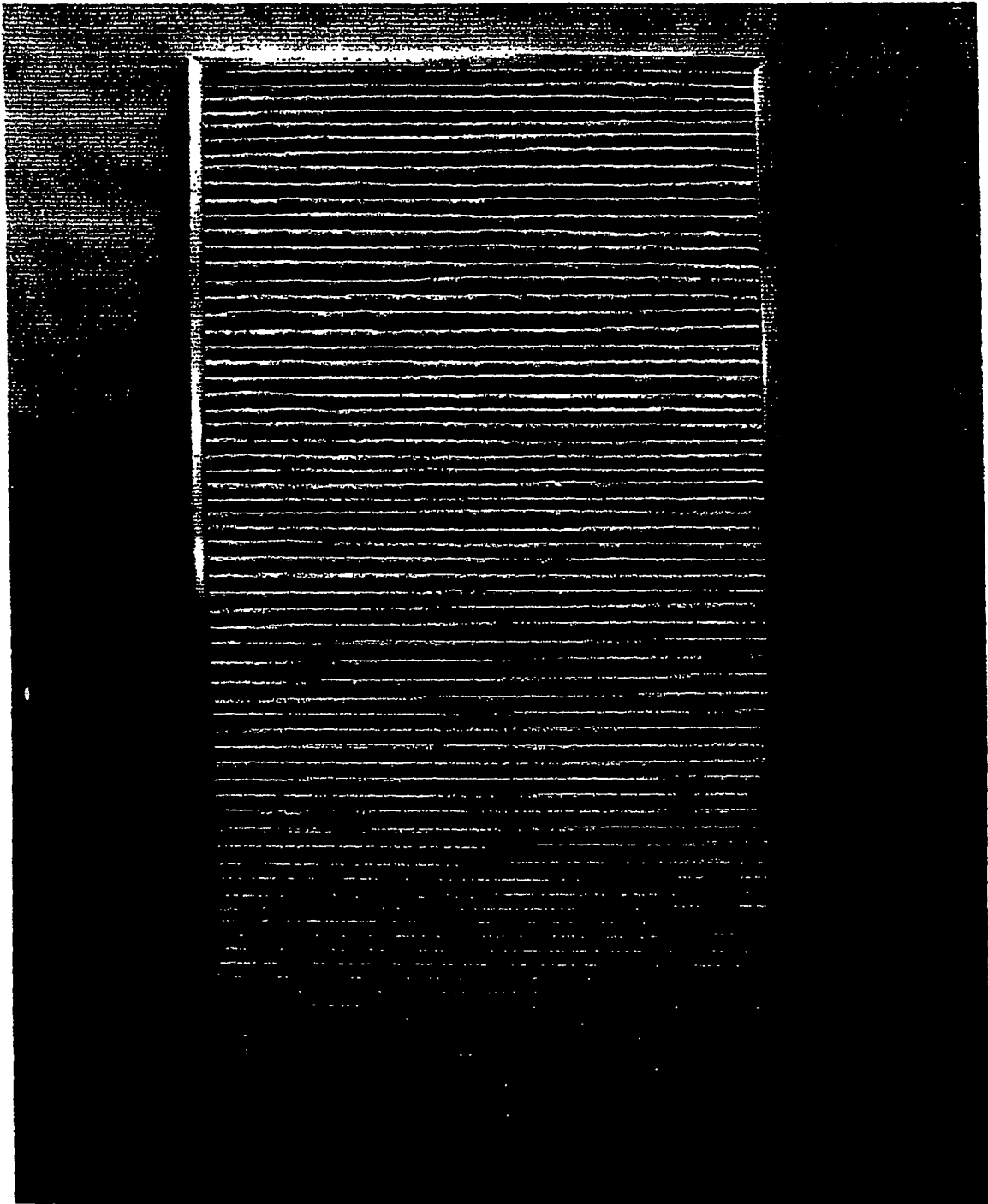


Fig. 8



Fig. 9

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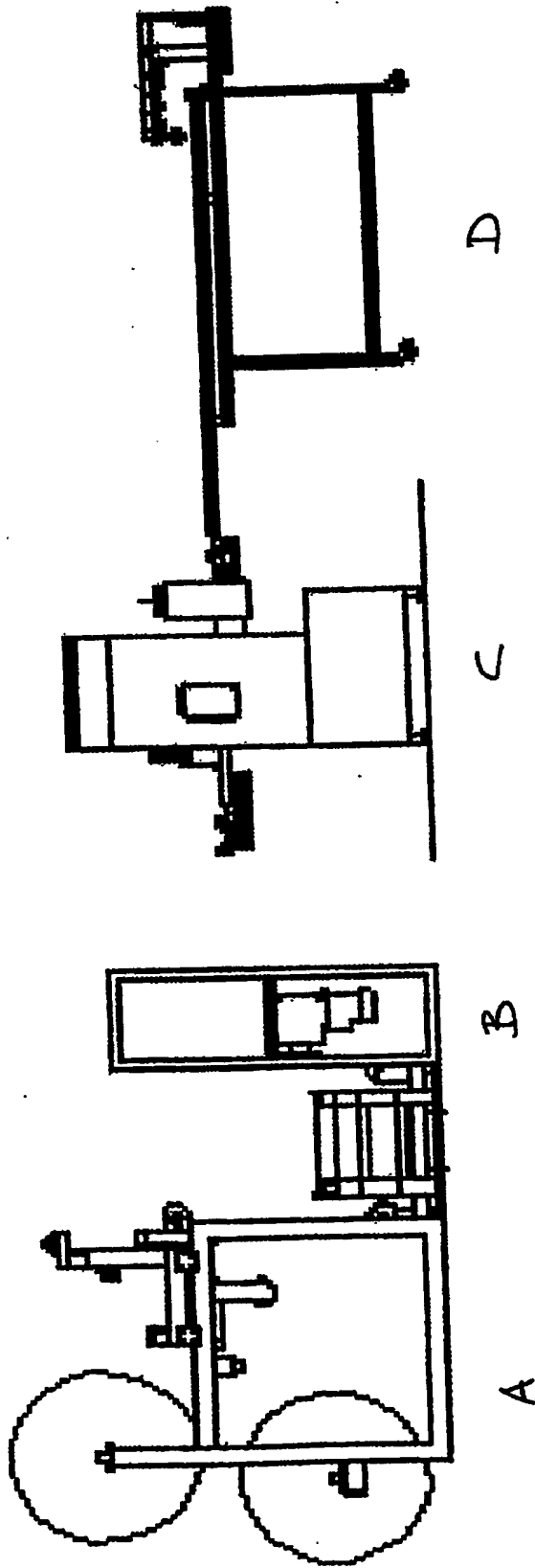


Fig II

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